

1-1-2004

# Higher Power Output in A PEMFC Operating Under Autonomous Oscillatory Conditions in the Presence of CO

J. X. Zhang

Ravindra Datta

Worcester Polytechnic Institute, rdatta@wpi.edu

Follow this and additional works at: <http://digitalcommons.wpi.edu/chemicalengineering-pubs>



Part of the [Chemical Engineering Commons](#)

---

## Suggested Citation

Zhang, J. X. , Datta, Ravindra (2004). Higher Power Output in A PEMFC Operating Under Autonomous Oscillatory Conditions in the Presence of CO. *Electrochemical and Solid State Letters*, 7(3), A37-A40.

Retrieved from: <http://digitalcommons.wpi.edu/chemicalengineering-pubs/23>

This Article is brought to you for free and open access by the Department of Chemical Engineering at DigitalCommons@WPI. It has been accepted for inclusion in Chemical Engineering Faculty Publications by an authorized administrator of DigitalCommons@WPI.



## Higher Power Output in a PEMFC Operating under Autonomous Oscillatory Conditions in the Presence of CO

Jingxin Zhang\* and Ravindra Datta\*\*<sup>z</sup>

Fuel Cell Center, Department of Chemical Engineering, Worcester Polytechnic Institute, Worcester, Massachusetts 01609, USA

Time-averaged cell voltage, cell efficiency, and power density in an autonomous oscillatory state was higher than that in stable steady-state for a proton exchange membrane fuel cell (PEMFC) operating in the presence of CO in the anode feed reformat gas. The average power density under such an oscillatory state at 55°C is twice that under a stable steady state. The average cell voltage and power density gain are due to the decrease of the time-averaged anode overpotential in the oscillatory state. This report thus provides experimental evidence that autonomous oscillatory operation of fuel cells in the presence of CO can increase the power output as compared to that in stable steady-state operation.

© 2004 The Electrochemical Society. [DOI: 10.1149/1.1643593] All rights reserved.

Manuscript submitted June 12, 2003; revised manuscript received September 15, 2003. Available electronically January 22, 2004.

Periodic or chaotic behavior has been observed in both homogeneous and heterogeneous reaction processes, and especially in electrochemical systems.<sup>1</sup> If such systems are well-mixed, only temporal periodic variations of the variables appear. Otherwise, spatiotemporal patterns may be observed, *e.g.*, in the concentration of adsorbed species on an electrode surface.<sup>2</sup> The literature is replete with reports of oscillatory phenomena in electrochemical systems, and the mechanistic understanding of the origin of such oscillations is being continually advanced.<sup>3-6</sup> Generally, the periodic behavior of an electrochemical system is due to the interplay of nonlinear electrode kinetics, mass transport, and the external electrical circuitry. The mathematical models for these phenomena contain nonlinear differential equations for reactant concentrations, coverage of surface species, and current or voltage as variables.

Oscillations in reaction systems were considered puzzling and largely irrelevant. Later, there was an effort to search for ways to exploit nonlinear kinetics.<sup>7,8</sup> For instance, the reaction rate is increased in a forced oscillatory biochemical reaction.<sup>9</sup> Similar phenomena were also observed in conventional chemical reactions with nonlinear kinetics.<sup>10</sup> In these examples it was demonstrated that efficiency could be improved by operating in a forced oscillatory state. With the improved theoretical understanding of periodic behavior in electrochemical systems, the expectations of their practical utility are also increasing.<sup>7,8</sup>

Recently, we found that sustained potential oscillations exist in proton exchange membrane fuel cells (PEMFCs) fed with H<sub>2</sub> containing low levels of CO when operated under constant current conditions.<sup>11</sup> The oscillations were determined to be due to the nonlinear kinetics of the anode reactions coupled with the mass and charge conservation. Here we present our findings on increased power output of PEMFCs when operated under such oscillatory conditions.

### Experimental

The experimental details can be found in our previous work.<sup>11</sup> In short, two pieces of electrode were bonded to either side of a solid polymer electrolyte membrane (Nafion 115). An electrode containing 0.35 mg/cm<sup>2</sup> PtRu (atomic ratio 1:1, E-TEK) was used at the anode, exposed to a simulated reformat gas (H<sub>2</sub> containing low levels of CO, also containing 20% CO<sub>2</sub> in some experiments). The cathode containing 0.4 mg/cm<sup>2</sup> Pt (E-TEK) was exposed to humidified O<sub>2</sub>. A membrane electrode assembly (MEA) with 5 cm<sup>2</sup> effective electrode area was prepared by hot-pressing at 130°C and under a pressure of 4000 lb for about 2 min. The MEA was tested in a single cell (Electrochem, Inc.) in a test station with temperature,

pressure, and mass flow control. The total pressure at both anode and cathode chamber was 30 psig. The volumetric flow rates reported in this study are all in units of standard (1 atm and 25°C) cubic centimeters per min (sccm). An electronic load (HP 6060B) interfaced with a PC was used to measure the current-voltage characteristics of the fuel cell.

### Results

The performance of a fuel cell in the laboratory may be experimentally evaluated under constant voltage, constant current, or constant resistance modes with an electronic load. We observed sustained potential oscillations when a fuel cell fed with H<sub>2</sub>/CO was operated under the constant current mode, with the anode catalyst being PtRu.<sup>11</sup> Since oscillations were not observed when the fuel cell was operated under the constant voltage or constant resistance modes, it is possible to directly compare the performance under an oscillatory state with that in a stable steady state.

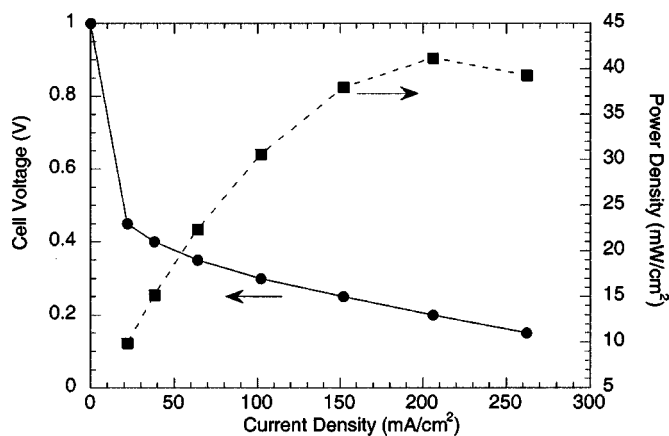
The fuel cell current-voltage relationship at room temperature obtained for a H<sub>2</sub> feed containing 100 ppm CO under constant voltage mode (stable steady-state) is shown in Fig. 1 along with the corresponding power output (in units of mW/cm<sup>2</sup>). Even though the open-circuit voltage is around 1.0 V, the cell voltage drops precipitously to 0.4 V, even when only a small current (*i.e.*, 30 mA/cm<sup>2</sup>) is drawn. Such a large initial drop in cell voltage is due to severe poisoning of the PtRu catalyst by CO at room temperature. The peak power output was only around 40 mW/cm<sup>2</sup>, which occurs at a current density of about 200 mA/cm<sup>2</sup>. When the fuel cell is operated in the constant current mode, the cell voltage begins to oscillate. The cell voltage pattern at three different constant current densities is shown in Fig. 2. The cell voltage oscillates over a wide range, and hence so does the power output, also shown in Fig. 2. The temporal variation of voltage and wattage are identical, because current is constant. Furthermore, because voltage efficiency,  $\epsilon_v = V/V_0$ , the ordinate in Fig. 2 also can be viewed as being proportional to efficiency. The amplitude and period of the oscillations at room temperature were larger than those at higher temperatures. This is consistent with our finding that the oscillatory behavior observed by varying the fuel cell temperature is due to a Hopf bifurcation.<sup>12</sup>

The time-averaged cell voltage and power density corresponding to Fig. 2 are plotted in Fig. 3. The time-averaged cell voltage does not change greatly as a function of current density. The time-averaged power output thus increases almost linearly with the current density in the range investigated. Further, the time-averaged cell voltage is substantially higher when compared to the stable steady-state value (Fig. 1). For example, at a current density of 200 mA/cm<sup>2</sup>, if the fuel cell were operated at a stable steady state, *i.e.*, in the constant voltage mode, the cell voltage is only about 0.2 V, while under the oscillatory state, the time-averaged cell voltage is almost 0.5 V. Thus, it is evident from a comparison of Fig. 3 and 1 that the time-averaged power output when operated under oscillation

\* Electrochemical Society Student Member.

\*\* Electrochemical Society Active Member.

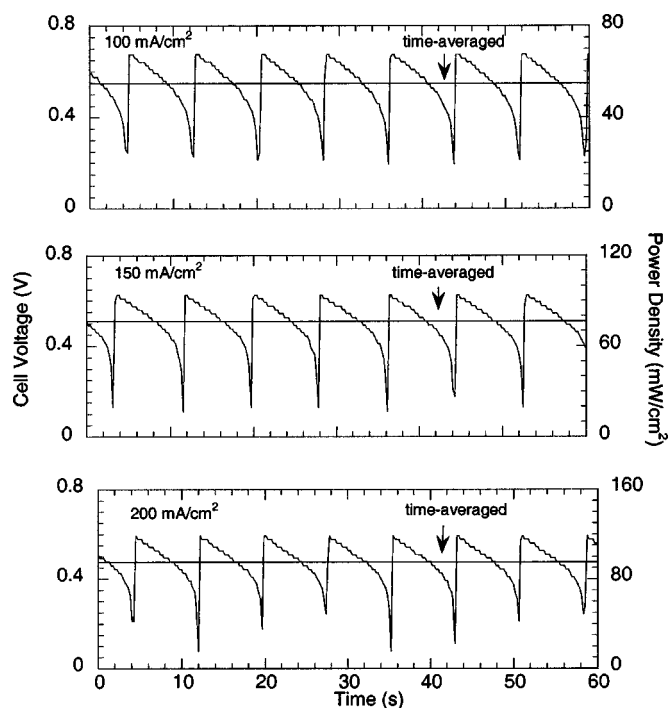
<sup>z</sup> E-mail: rdatta@wpi.edu



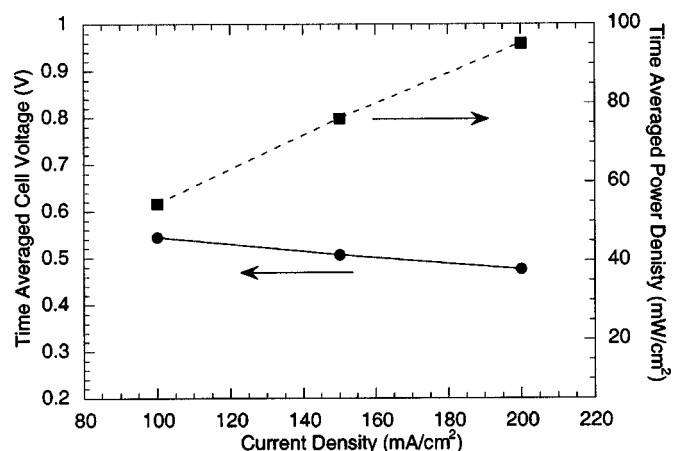
**Figure 1.** Cell voltage and power output at different current densities at stable steady-state (constant voltage mode) at room temperature. Anode feed:  $\text{H}_2/100$  ppm CO; anode inlet flow rate: 60.1 sccm; cathode feed:  $\text{O}_2$ .

tory conditions is substantially higher than that under stable conditions. Similar results were obtained for a  $\text{H}_2$  feed containing 100 ppm CO and 20%  $\text{CO}_2$ , as well as for a  $\text{H}_2$  feed containing 200 ppm CO.

The performance of the fuel cell operated with a  $\text{H}_2/108$  ppm CO anode feed under stable steady-state conditions (constant voltage mode) at different temperatures is summarized in Fig. 4. The fuel cell performance is poor at low temperatures. Further, no limitation imposed by transport of reactant gases is evident from the polarization curves in the current density range investigated. The corresponding power density is plotted in Fig. 5. The power output improves with the increase of fuel cell temperature, which is attributable to both reduced CO affinity for the catalyst surface, as



**Figure 2.** Cell voltage and power density at different current densities in autonomous oscillatory state (constant current mode). The solid straight line indicates the time-averaged value of both cell voltage and power density. The other conditions are the same as in Fig. 1.



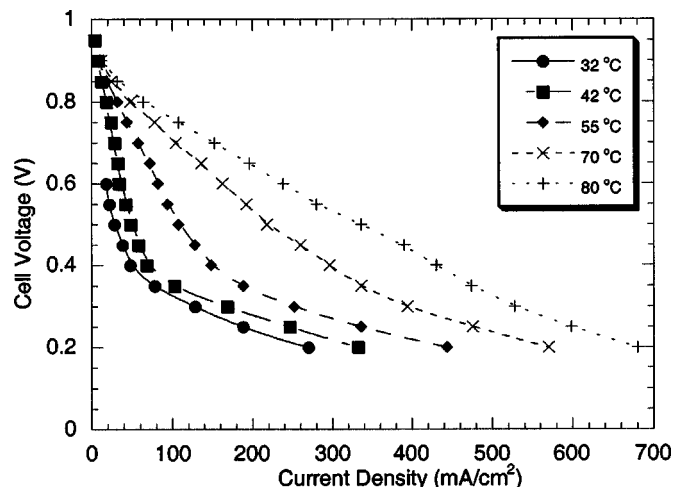
**Figure 3.** Time-averaged cell voltage and power output at different current densities in autonomous oscillatory state (constant current mode) at room temperature. The other conditions are the same as in Fig. 1.

well as enhanced  $\text{H}_2$  and CO electro-oxidation rates.<sup>11</sup> The peak power output thus, at 55°C is about 90  $\text{mW}/\text{cm}^2$ , while the peak power density at 80°C is about 180  $\text{mW}/\text{cm}^2$ .

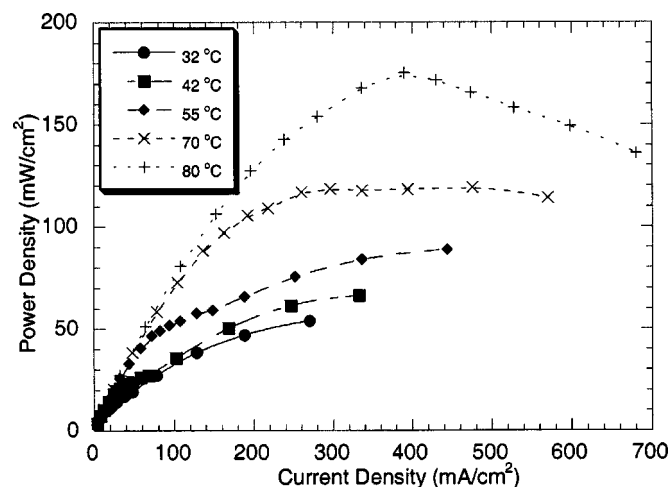
Figure 6 shows the time-averaged cell voltage and power density under the autonomous oscillatory state at a fuel cell temperature of 55°C. The average cell voltage decreases gradually with the current density, and is higher than that in Fig. 4 for the same current density. The time-averaged power density in the oscillatory state shown in Fig. 6 is nearly double when compared to that in Fig. 5 at 55°C (*i.e.*, 150–200  $\text{mW}/\text{cm}^2$  vs. about 90  $\text{mW}/\text{cm}^2$  maximum). This power output is even higher than the maximum at 80°C for the stable steady state. Moreover, the power output at 55°C in the oscillatory state shown in Fig. 6 may not have peaked yet.

## Discussion

Autonomous oscillations were observed at temperatures below about 70°C.<sup>11</sup> A quantitative mechanistic model and analysis has been given by us before.<sup>11,12</sup> Qualitatively, when CO builds up on the catalyst surface, *i.e.*, as  $\theta_{\text{CO}}$  increases, the anode becomes increasingly polarized to a higher potential to compensate for a smaller  $\theta_{\text{H}}$  and to sustain the applied constant current. The anode overpotential increase accelerates the electro-oxidation of  $\text{CO}_{\text{ad}}$  on



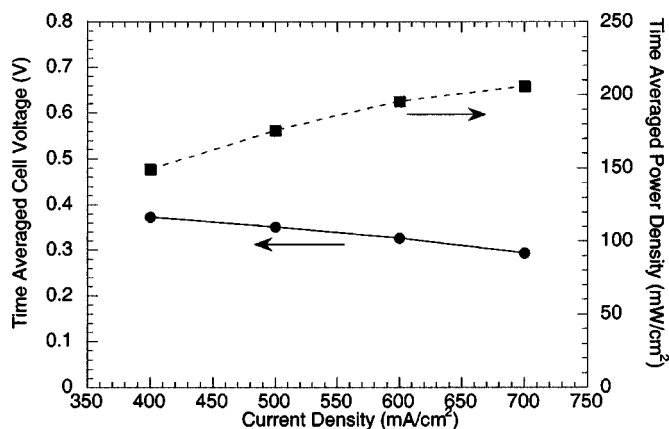
**Figure 4.** Polarization curves at stable steady-state (constant voltage mode) for various cell temperatures. (•) 32, (■) 42, (◆) 55, (×) 70, and (+) 80°C. Anode feed:  $\text{H}_2/108$  ppm CO; anode inlet flow rate: 48.1 sccm.



**Figure 5.** Power output of stable steady-states (constant voltage mode) for various cell temperatures shown in Fig. 4.

the catalyst surface via oxygen-containing surface species such as  $\text{OH}_{\text{ad}}$ , which is formed more readily on the catalyst surface at higher overpotentials. When the CO electro-oxidation rate exceeds the rate of CO adsorption, the surface coverage of CO,  $\theta_{\text{CO}}$ , declines. This happens quickly beyond a critical overpotential. Thus,  $\theta_{\text{H}}$  increases and  $\text{H}_2$  oxidation reaction sustaining the current is no longer constrained by  $\theta_{\text{CO}}$ . The anode overpotential, thus, drops quickly to a low value. However, this drop in the potential recreates a situation where the rate of CO adsorption exceeds that of CO electro-oxidation. Therefore, CO molecules begin to build up again on the catalyst surface and the electrode must again be polarized increasingly to a higher overpotential. Thus, the cycle repeats itself. The conditions for oscillatory state operation may change depending upon the cell temperature and composition of the reformat feed stream. The poisoning species in reformat may not necessarily be CO for oscillations to appear. Rather any species that blocks the catalyst surface at low overpotentials and can be electro-oxidized at high overpotentials could conceivably cause oscillatory behavior.

Self-organized potential oscillations occur at conditions far from thermodynamic equilibrium with the presence of appropriate feedback loops.<sup>3</sup> As discussed above, the dynamic instability is linked to the interplay of the electrode kinetics and the external electrical circuit trying to sustain a constant current. A negative differential resistance ( $\partial V/\partial i < 0$ ), *i.e.*, when the total current decreases with



**Figure 6.** Time-averaged cell voltage and power output at different current densities in autonomous oscillatory state (constant current mode).  $T_{\text{cell}} = 55^\circ\text{C}$ ; anode feed:  $\text{H}_2/108$  ppm CO; anode inlet flow rate: 48.1 sccm.

an increase of electrode potential, is necessary for the existence of electrochemical instability, which has been shown to exist in the anode potential oscillations in this study.<sup>12</sup> The following processes have been identified as essential for the occurrence of these oscillations<sup>12</sup>: (i) a current carrying process (H electro-oxidation, which depends upon the anode overpotential); (ii) a process responsible for the occurrence of the negative differential resistance (potential-dependent adsorption and desorption of OH); and (iii) a potential-dependent process in which potential has a positive effect on the reaction rate (reactive removal of CO). The temporal evolution of the anode reaction system is explained quantitatively by the differential equations derived from charge as well as mass balance. By applying the linear stability analysis, *i.e.*, by the sign of the eigenvalues of the associated Jacobian matrix of the linearized equations governing the system, a Hopf bifurcation has been shown to exist in this system.

The oscillatory fuel cell voltage reflects the sustained effort for self-recovery on part of the catalyst surface to maintain a given current. The increased power output in the oscillatory state is evidently caused by the time-averaged cell voltage increase at a given current density. The increased average cell voltage is a result of the decreased average anode overpotential. It has been shown computationally and experimentally that under oscillatory state, the rise and fall of overpotential in a cycle is not symmetrical about the unstable steady-state value. The deviation of the minimum overpotential is larger than that of the maximum overpotential.<sup>12</sup> Furthermore, for a large fraction of the time in a cycle, the anode overpotential is at a lower value than that under a stable steady state. Such a gain in the decrease in anode overpotential for a substantial fraction of the time in a cycle leads to the higher average cell voltage in the oscillatory state.

The increased power output in the oscillatory state is consistent with the oscillations appearing due to the effort by the system to maximize the entropy production rate  $\sigma_s$ .<sup>9</sup> In the fuel cell system, this is equal to current (reaction rate) times cell potential (which is proportional to the affinity of the reaction system).<sup>13</sup> The relation is shown by the following equation

$$\sigma_s = \frac{1}{T} Ar = \frac{zF}{T} Vi \quad [1]$$

where  $\sigma_s$  is the entropy production rate,  $T$  is temperature,  $A$  is the affinity,  $r$  is the reaction rate,  $z$  is the number of electrons in the reaction,  $F$  is the Faraday constant,  $V$  is cell voltage, and  $i$  is the current. Thus, the rate of entropy production in a fuel cell is nothing but the rate of power production. We have shown that the phase angles of variables such as the surface coverage of CO, H, and OH are different.<sup>12</sup> Phase lag among variables leads to different phase angles between the reaction rate (current) and affinity (voltage) of the system. This phase relation between affinity and reaction rate is another factor in determining the power output of a system.<sup>7,14</sup>

There has been an attempt to accelerate reaction rate or decrease the oxidation potential for the electro-oxidation of formic acid by forced oscillation, *i.e.*, by superimposing a periodic potential<sup>15</sup> or current signal<sup>16</sup> with a certain amplitude and frequency on the stable potential or voltage. In a certain range of frequency used, either the oxidation current is increased or the overpotential is decreased, implying an advantage of forced oscillatory operation over stable steady-state operation.<sup>15,16</sup> The gain in both reaction rate and efficiency has been demonstrated in biological reactions as well, where the biochemical reaction system exhibits autonomous oscillations.<sup>7,9</sup> A perturbation to one of the reactants (*i.e.*, oxygen influx) in the form of a sinusoidal wave was used instead of steady flux. It was found that several of the thermodynamic quantities were changed as compared to the undisturbed state. The phenomenon is believed to be due to resonance, which is a generic feature of oscillatory systems. Reaction rate enhancement in other chemical reaction systems has also been observed via forced concentration oscillations of reactants.<sup>17</sup> There is a significant improvement of the time-averaged

production rate relative to optimal steady-state operation for nonlinear kinetics, while for linear kinetics there is no improvement.<sup>17</sup>

While advantages are reported for these forced oscillatory reactions, almost all the examples demonstrated so far need an external oscillatory signal to force the reaction system into an oscillatory state. However, results reported here provide evidence that a system operating under an autonomous oscillatory condition also shows power output gains as compared to that at a stable steady state under otherwise identical experimental conditions. Although the periodic forcing of the external parameters (*e.g.*, reactant flow rates, current, or cell voltage) may not be difficult in an energy conversion device such as a fuel cell, cumbersome external control for periodic forcing is generally undesirable. Thus, our observation may be useful in managing power output for fuel cells, where the control of cell or stack current is not difficult. Although the periodic nature of voltage output would generally be undesirable, it is not a significant problem to condition this with modern electronic circuitry. Furthermore, the overall stack voltage may actually be less periodic, perhaps approaching the total average value due to the phase angle difference in cell voltage of the single oscillator (single cell) within a stack.

Undoubtedly, raising the cell temperature can increase the power output of a fuel cell operating under a stable steady state. However, the PEMFC operating temperature usually cannot exceed about 80-90°C due to limitations imposed by the current polymer electrolyte membrane. Thus, utilizing the oscillatory kinetics may serve as an alternative approach to improving the power output (and thus managing CO poisoning) of a reformate-fed fuel cell. However, even in the oscillatory state operation, the power output is not comparable to that with pure hydrogen. Nevertheless, the present results provide evidence that operation under autonomous oscillatory conditions (due to the inherent nonlinear kinetics in electrode reactions) can increase the power output as compared to that under a stable steady-state operation in an energy conversion device. This has been expected and hoped for by researchers working on nonlinear dynamics in electrochemical systems.<sup>8</sup>

## Conclusions

A PEMFC can be operated in an autonomous oscillatory state under constant current conditions when reformate is used as the anode feed. Compared to the stable steady-state operation, the time-averaged cell voltage, efficiencies, and power density are higher under the oscillatory state. The increase in average cell voltage and power density is due to the decrease of the time-averaged anode overpotential under oscillatory conditions. There are relatively sharp bursts in the anode overpotential only periodically to rid the surface of the poisoning species. These observations may be useful for developing an operational strategy for improved management of power output in PEMFCs in the presence of CO.

## Acknowledgment

J.Z. gratefully acknowledges the Dr. Chue-san Yoo Fellowship.

Worcester Polytechnic Institute assisted in meeting the publication costs of this article.

## References

1. G. Ertl, *Science*, **254**, 1750 (1991).
2. Y. J. Li, J. Osolonovitch, N. Mazouz, F. Plenge, K. Krischer, and G. Ertl, *Science*, **291**, 2395 (2001).
3. K. Krischer, in *Modern Aspects of Electrochemistry*, J. O'M Bockris, B. E. Conway, and R. E. White, Editors, Vol. 32, p. 1, Plenum Press, New York (1999).
4. J. L. Hudson and T. T. Tsotsis, *Chem. Eng. Sci.*, **49**, 1493 (1994).
5. M. T. M. Koper, *Adv. Chem. Phys.*, **92**, 161 (1996).
6. P. Strasser, *Electrochem. Soc. Interface*, **9**(4), 46 (2000).
7. J. G. Lazar and J. Ross, *Science*, **247**, 189 (1990).
8. P. Strasser, Ph.D. Thesis, Freie Universitat Berlin, Berlin (1999).
9. J. G. Lazar and J. Ross, *J. Chem. Phys.*, **92**, 3579 (1990).
10. M. Schell, H. M. Schram, and J. Ross, *J. Chem. Phys.*, **88**, 2730 (1988).
11. J. Zhang and R. Datta, *J. Electrochem. Soc.*, **149**, A1423 (2002).
12. J. Zhang, J. D. Fehribach, and R. Datta, *J. Electrochem. Soc.*, To be published.
13. I. Prigogine, *Introduction to Thermodynamics of Irreversible Processes*, p. 31, Interscience Publishers, New York (1961).
14. P. H. Richter and J. Ross, *Science*, **211**, 715 (1981).
15. R. R. Adzic, K. I. Popov, and M. A. Pamic, *Electrochim. Acta*, **23**, 1191 (1978).
16. M. Schell, F. N. Albahadily, and J. Safar, *J. Electroanal. Chem.*, **353**, 303 (1993).
17. J. Thullie, L. Chiao, and R. G. Rinker, *Chem. Eng. Sci.*, **42**, 1095 (1987).